

# Magnetically controllable generation of ferrofluid droplets

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**Abstract** This paper reports the manipulation of ferrofluid droplets by using a microfluidic flow-focusing device equipped with a magnetic tweezer. Besides the traditional flow rate controlling method, the magnetic field also can be applied to control the size of the droplets. Two major effects in magnetic manipulation process: magnetoviscous effect and magnetic drag effect, were studied. Under a fixed flow rate (CP = 1 mL/h, DP = 0.2 mL/h), the average sizes of ferrofluid droplets were tunable from 135 to 95  $\mu\text{m}$  by varying the magnetic field from 0 to 60 mT. Moreover, square wave magnetic field can be used to periodically generate droplets with different sizes. These results are helpful to understand the generation mechanism of the ferrofluid droplet and supply a novel method for manipulating droplets with a predetermined size and distribution.

**Keywords** Microfluidic · Magnetic · Ferrofluid · Flow-focusing · Droplets

## 1 Introduction

Manipulation of small volumes liquid is important in miniaturized biological and chemical analysis, since less

sample means faster reaction and lower cost. In this case, droplet-based microfluidics were developed to create discrete volume based on immiscible phases (Huebner et al. 2008; Song et al. 2006; Teh et al. 2008). In contrast to continuous flow, droplets can be individually transported, mixed and analyzed (Fair 2007; Link et al. 2006). Droplet microfluidic has the ability to process a mass of reactions at the same time without increasing device complexity. With the benefit of droplet microfluidics, large number of applications in the area of biochemical and material science like synthesis of polymer particles (Jeong et al. 2005; Nie et al. 2006), drug delivery (Ruge and Rusetski 1993) and diagnostic testing (El-Ali et al. 2006) were realized. Therefore, controllable droplet generation and manipulation are important research topics.

There are two basic styles, passive and active, for generating the droplet. Passive methods generate and manipulate the droplets by varying the microchannel structures such as T-junction (Nisisako et al. 2002; Priest et al. 2006; Thorsen et al. 2001; Xu et al. 2006) and flow-focusing (Anna et al. 2003; Tan et al. 2006; Woodward et al. 2007; Yobas et al. 2006). Although this method has the advantage of easy fabrication, it lacks flexibility due to fixed microchannel configurations. Active methods usually combine channel structure with external sources. Electric (Abdelgawad and Wheeler 2009; Jebrail et al. 2012; Srinivasan et al. 2004; Velev et al. 2003), magnetic (Nguyen 2011; Pippert et al. 2007; Zhang et al. 2009), acoustic (Schmid and Franke 2013), optical (Diguet et al. 2009) and temperature fields (Baroud et al. 2007; Nguyen et al. 2007) are most frequently used. For the active methods, the fabrication of chip is rather complex and several bulky equipments are usually needed. To this end, an ideal droplet manipulation method should be simple in fabrication and easy in control. Among the mentioned active methods, magnetic

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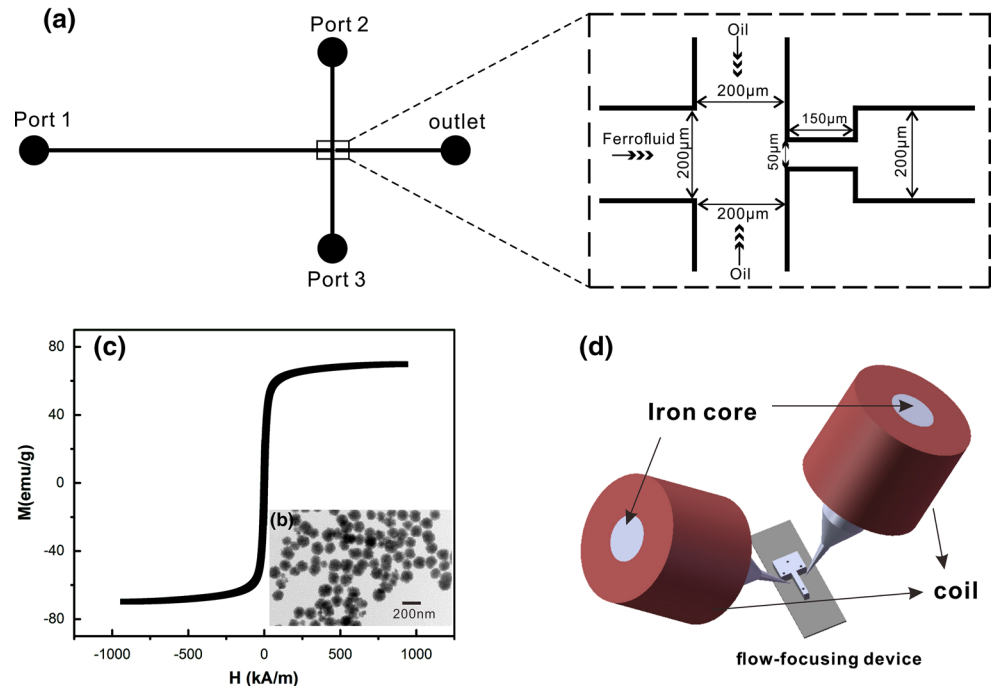
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**Fig. 1** **a** Schematic of the microfluidic device. Ferrofluid droplets are formed in a microfluidic flow-focusing junction. **b** TEM image and **c** magnetization curve of  $\text{Fe}_3\text{O}_4$  nanoparticles. **d** Local field applied by magnetic tweezer device



manipulation technique has the advantage of easy realization. It could not be affected by experimental environment like pH, ionic or surface charge. With these benefits, this method was favorable.

Ferrofluids are most commonly used magnetic droplet phase. Several works were devoted to the formation mechanism of ferrofluid droplets. Tan et al. (2010) firstly reported the influence of magnet position in microfluidic T-junction. When the magnet was placed upstream, droplet size increased with increasing the magnetic flux density. In contrast, when magnet was placed downstream, droplet size decreased (Tan et al. 2010). Role of homogeneous magnetic field was also studied (Tan and Nguyen 2011; Wu et al. 2013). Both radial and axial magnetic fields can actively control the formation of ferrodroplets in flow-focusing configuration. In general, the two kinds of magnetic fields facilitate the formation of larger droplets. Furthermore, a numerical study (Liu et al. 2011) for axial homogeneous magnetic field-controllable ferrofluid droplet generation clearly showed the inner flow structure throughout the whole formation process. However, the influence of local field and programmable magnetic signal in flow-focusing device on the droplet size and formation mechanism in squeezing regime is still missing.

Here, we present a microfluidic chip-based continuous magnetic droplet generation method for quickly controlling the size of ferrofluid droplets. External local magnetic field generated by magnetic tweezer device was applied perpendicular to the upstream microchannel. We demonstrate that the applied magnetic field leads to a versatile and reliable modulation of droplet size in the squeezing

regime of production. Magnetoviscous effect and magnetic drag effect are studied to give a clear understanding of droplet breakup dynamics. Square wave magnetic field can be used to periodically generate droplets with different sizes.

## 2 Experiment

### 2.1 Device fabrication

The microfluidic devices were fabricated using standard soft lithography (Duffy et al. 1998). First, a layout editor (CorelDRAW) was used to design the devices. The schematic and dimensions of flow-focusing configurations used in the experiments are shown in Fig. 1a. Next, a master mold was fabricated using the negative SU-8 photoresist (SU-8-2050, MicroChem). The thickness of the mold, which defines the rectangular channel depth, is 100  $\mu\text{m}$ . Polydimethylsiloxane (PDMS) mixture (10 A:1 B) was then poured onto the master mold. After degassing in a vacuum desiccator for 20 min, it was cured in an 80  $^{\circ}\text{C}$  convection oven for 30 min. Then, the cast PDMS was peeled from the SU-8 mold and punched using a manual puncher (Harris Uni-Core, World Precision Instruments). Fluidic access holes with a diameter of 1.2 mm were created. The cast PDMS was then washed in ethanol for 5 min followed by rinsing in distilled water. After the cleaning process, the PDMS parts were then placed in an oven at 80  $^{\circ}\text{C}$  for 10 min to ensure that the surface was free of water. Finally, oxygen plasma treatment (WH-1000, Wenhao) was used to

bond the device. Before use, the chips were left at 65 °C for 24 h to ensure full recovery of the PDMS hydrophobicity.

## 2.2 Synthesis of superparamagnetic nanoparticles

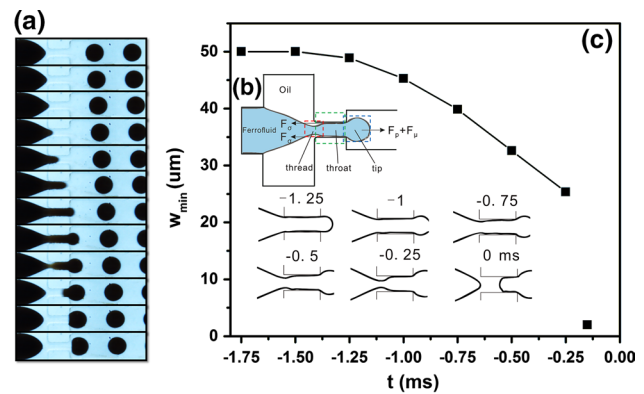
Superparamagnetic  $\text{Fe}_3\text{O}_4$  nanoparticles (see example in Fig. S1†) were synthesized by the solvothermal method. Briefly,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  (1.08 g), NaAc (4.0 g) and PAA (100 mg) were dissolved in ethylene glycol (10 mL) and diethylene glycol (30 mL) under magnetic stirring. The obtained homogeneous yellow solution was transferred to a Teflon-lined stainless steel autoclave and sealed to heat at 200 °C. After reaction for 12 h, the autoclave was cooled to room temperature. The obtained magnetic particles were washed with ethanol and water four times, respectively. Then they were dried into a powder under vacuum and dispersed in deionized water with 30 % mass concentration. All magnetic solutions were redispersed under ultrasound for 5 min before use. Figure 1b, c shows the TEM image and magnetization curve of  $\text{Fe}_3\text{O}_4$  nanoparticles.

## 2.3 Experimental setup and procedure

The uniform magnetic field was generated using a magnetic tweezer (Rich et al. 2011) with 1500-turn coil assembled around an iron core. A separation gap of 7 mm ensures that the generated magnetic field is homogeneous and uniform. Next, the microfluidic devices were positioned in the middle of the gap (Fig. 1d). The channel of the dispersed phase is aligned perpendicular to the magnetic field. The magnetic flux densities were measured using a commercial gaussmeter (HT20, Cestsen) with an accuracy of  $\pm 2\%$ . A DC power source (selfmade, can be programmed) was used to vary the magnitudes of the magnetic flux density by changing the applied electric current. A high-speed camera (FASTCAM SA5 1000 k-M3, Photron) was used to capture the droplet formation process. Two syringe pumps (LSP02-1B, LongerPump) were used to deliver the fluids through polyethylene (Smiths medical, 0.38 mm ID, 1.09 mm OD) into the microfluidic devices (see example in Figs. S2†, S3†).

Images of the droplet formation process were acquired at a rate of 4000 frames per second. Sizes of ferrofluid droplets were evaluated using customized image processing software ImageJ. The produced ferrofluid droplets are monodispersed with a polydispersity (defined as the standard deviation of the droplet size divided by the average droplet size) of  $< 5\%$ . The magnetic flux density of the electromagnet can be varied by changing the supply current.

In our experiment, deionized water and water-based ferrofluid were employed as the dispersed phase to form droplets in plant oil phase. At 25 °C, the density of the ferrofluid



**Fig. 2** a Formation sequence of ferrofluid droplets in squeezing regime (time interval of each snapshot is 0.5 ms, CP = 1 mL/h, DP = 0.2 mL/h). b Various forces the ferrofluid tip suffered in droplet formation progress in the flow-focusing channel. c Evolution of minimal width  $w_{\min}$  of the thread and optical micrographs of the ferrofluid–oil interface along the breakup trajectory (CP = 1 mL/h, DP = 0.2 mL/h)

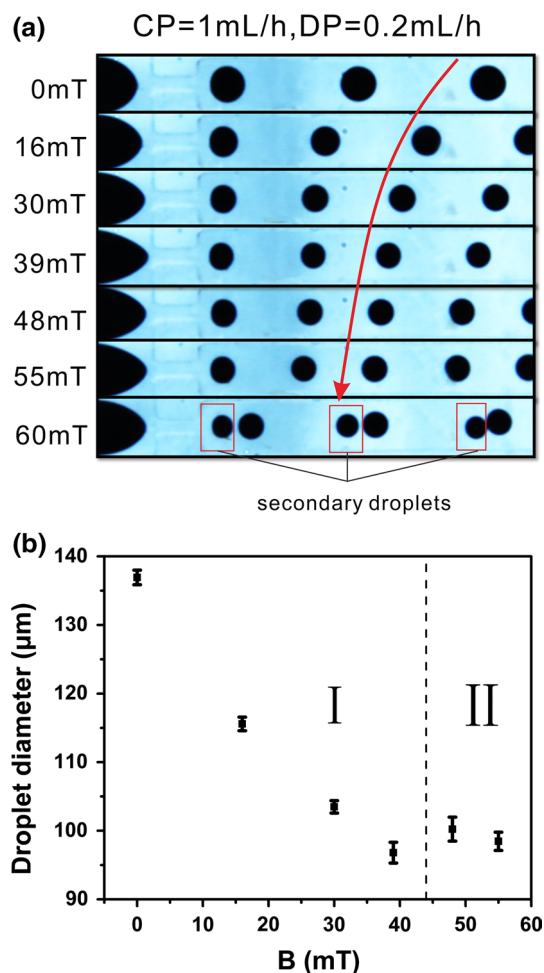
is  $1333 \text{ kg/m}^3$ . The density and viscosity of deionized water are  $995 \text{ kg/m}^3$  and  $0.8 \text{ mPa s}$ , respectively. A plant oil (Golden dragon fish) is used as the continuous phase. The density and viscosity of the plant oil are  $796 \text{ kg/m}^3$  and  $50 \text{ mPa s}$ , respectively. The interfacial tension between the ferrofluid and the plant oil is approximately  $1.56 \text{ mN/m}$ . The interfacial tension between water and the plant oil is approximately  $1.22 \text{ mN/m}$ .

## 3 Results and discussion

### 3.1 Effect of magnetic field on the formation of ferrofluid droplets

In flow-focusing geometry, depending on the properties of immiscible liquids and flow rates of inner and outer phases, droplets occurred in three different modes: squeezing, dripping and jetting (Nie et al. 2008). In the squeezing and dripping regime, the thread of the inner phase broke either in the throat or in the close proximity of the throat. In the jetting regime, a continuous thread of the inner phase extended into the outlet channel and broke far downstream of the throat.

In our experiment, most processes were happened in the squeezing regime and the others were in dripping or higher mode behaviors between squeezing and dripping (secondary droplet phenomenon shown in Fig. 3a). Figure 2a shows the typical preparation of ferrofluid droplet in a squeezing mode. Without applying the magnetic field, ferrofluid and oil start to flow in the chip under the pressure supplied by syringe pumps. Then they meet at the cross-junction and



**Fig. 3** **a** Ferrofluid droplet micrograph sequences under various magnetic flux densities. The *red arrow* shows the tendency of the droplet size and frequency with the increasing in outer magnetic field. **b** Sizes of ferrofluid droplets as a function of magnetic flux density. The *dash lines* are given for visual guidance

enter the orifice. Oil phase flows through the space around ferrofluid. In this process (Fig. 2b), viscous force  $F_{\mu}$  (caused by the viscous stress acting on the interface) and hydrostatic pressure  $F_p$  are the main reason leading to the collapse of ferrofluid thread. On the contrary, the interfacial tension force  $F_{\sigma}$  keeps the ferrofluid tip from moving forward. The balance of the three forces determines the breakup of the droplet. In squeezing regime, because the ferrofluid occupies almost the entire throat, pressure of continuous phase increases dramatically at the region outside ferrofluid thread, and the breakup process can be described by three stages (Garstecki et al. 2005) (Fig. 2c). First, the thread enters the orifice and the width  $w_{\min}$  of the neck stays constant. Second, a clearly visible neck develops and the thread collapses at a constant rate. In the third stage, the thread collapses rapidly, breaks and retracts upstream of the orifice, and the whole process starts again.

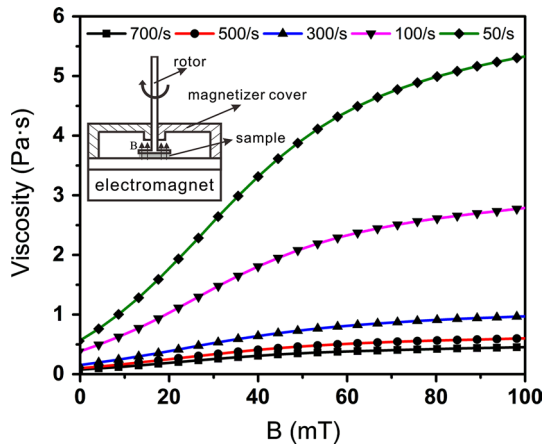
In this process, interfacial tension force is larger than viscous force. Capillary number ( $Ca = v\mu/\gamma$ , where  $v$  is the velocity of the continuous phase,  $\mu$  its viscosity, and  $\gamma$  the interfacial tension) is used to express the relative strength of the two. In squeezing regime, the  $Ca$  is low, and the hydrostatic pressure  $F_p$  is the key parameter of breakup. In dripping regime, ferrofluid occupies a fraction of space of the throat, continuous phase can flow through the orifice easily without a dramatic change of pressure, and thus  $F_{\mu}$  combining with  $F_{\sigma}$  determines the breakup of droplet. The thread maintains a constant shape, with the pump of inner phase, tip starts to grow, and  $F_{\mu}$  stretches the tip moving downstream until the weaker  $F_{\sigma}$  is no longer strong enough to hold the tip. To this end, the droplet is formed.

To investigate the influence of magnetic flux density, a local magnetic field ( $B = 0, 16, 30, 39, 48, 55, 60$  mT) was applied in the upstream of flow-focusing junction. The flow rate was fixed ( $CP = 1$  mL/h,  $DP = 0.2$  mL/h). Figure 3b shows the diameters of the formed ferrofluid droplets in the flow-focusing geometry under different magnetic field  $B$ . If  $B$  is smaller than 40 mT (Fig. 3b, area I), diameter of droplets decreases with the increasing in  $B$ . In comparison with the former works using axial or radial homogeneous global field (Tan and Nguyen 2011; Wu et al. 2013), local magnetic field played an opposite role in controlling the droplet size. Further increasing the magnetic flux density (Fig. 3b, area II), the average size of droplets stops changing and it almost keeps as a constant around 100  $\mu\text{m}$ . Finally, when  $B$  reaches 60 mT, the droplets are no longer monodisperse, and secondary droplets are presented (geometry-determined capillary instability, Shui et al. 2009) (Fig. 3a). Clearly, magnetic field plays an important role in controlling the generation of ferrofluid droplets. The average sizes of the droplets were tunable from 135 to 95  $\mu\text{m}$  by varying the magnetic field from 0 to 60 mT. Moreover, the size of the magnetic droplets can also be tuned by the flow rate, similar to the traditional flow rate controlling method. Therefore, this magnetic controlling method presents bi-mode controllability. Since magnetic control mode does not rely on the whole flow rate, it would be very important in many applications which need a stable flow rate.

### 3.2 Formation mechanism for the magnetically controllable droplets

Here, the detailed magnetically controllable mechanism was discussed. As soon as the magnetic field was added on the device, both the magnetoviscous effect and magnetic drag were presented.

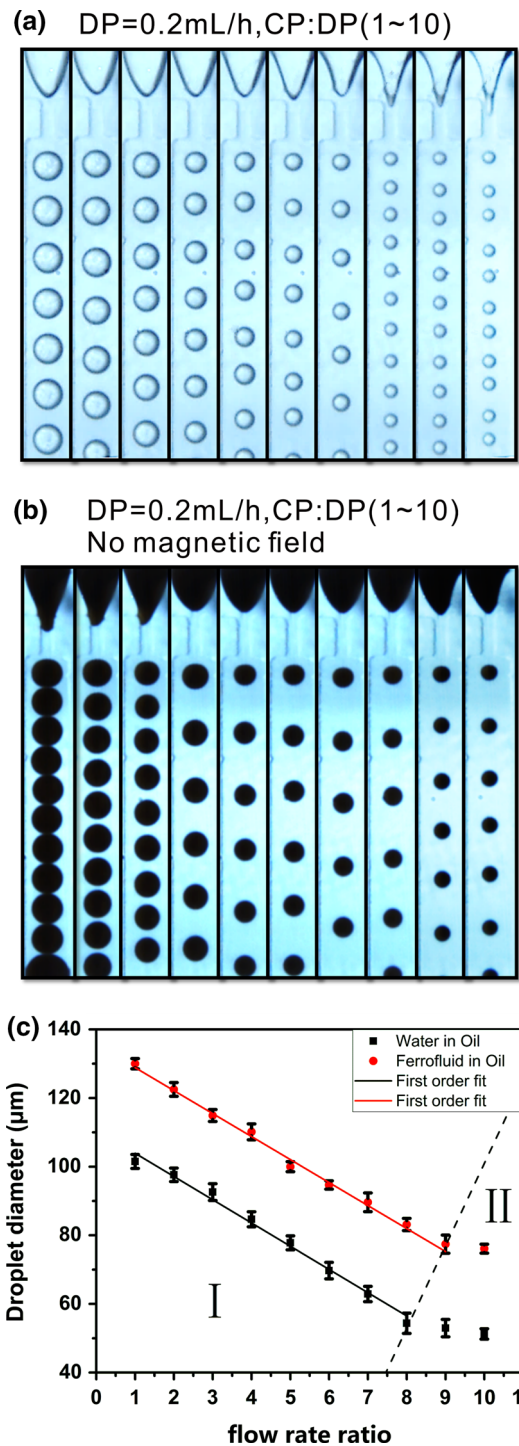
Under magnetic field,  $\text{Fe}_3\text{O}_4$  nanoparticles arranged to form chains-like structure along the direction of magnetic field (see example in Fig. S4†), and the viscosity of ferrofluid was changed. Figure 4 shows this magnetically



**Fig. 4** Rheological test curve of ferrofluid. Viscosity of ferrofluid increases with applied magnetic field at fixed shear rate. The inset is the sketch of the Physica MCR301 test system

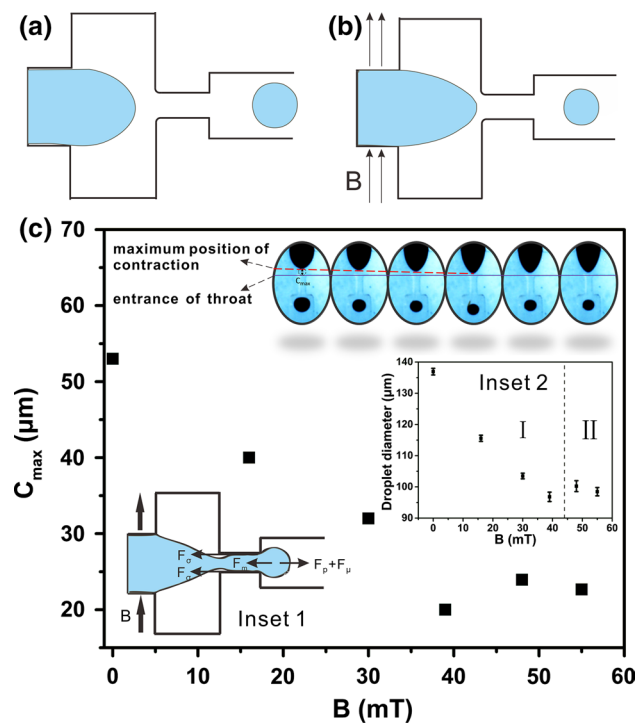
dependent viscosity of the ferrofluid tested by a commercial rheometer Physica MCR301 (produced by Anton Paar GmbH, Austria) equipped with an electromagnetic accessory MRD180. The sketch of the test system is shown in the inset of Fig. 4. The ferrofluid sample is placed between an electromagnet substratum and an upper rotatable non-magnetism flat rotor. The magnetizer cover is used to strengthen the magnetic field and make it uniform in the area of sample. In general, viscosity of ferrofluid increases with increasing in the magnetic flux density under a fixed shear rate.

To investigate the influence of inner phase viscosity, we compared water and ferrofluid droplets at the same flow condition. Figure 5 illustrates the effect of the value of  $Q_o/Q_i$  (flow rate ratio of outer phase and inner phase) on the size of water and ferrofluid droplets, and droplet sequences of this system, respectively. In this experiment, the flow rate of inner phase ( $Q_i$ ) was kept as a constant (0.2 mL/h). With the increasing in the ratio of the flow rate of immiscible liquids, the droplet diameters decrease (Fig. 5c, area I). The decrease is approximately linear on  $Q_o/Q_i$  which means shear mechanism induced strong dependence of droplet diameter and flow rate ratio (Nie et al. 2008). In squeezing regime, the whole formation process of droplets is dominated by hydrostatic pressure  $F_p$  and interfacial tension force  $F_\sigma$ . Inner phase blocks the throat, the buildup of  $F_p$  in continuous phase squeezes inner phase thread, and a neck evolves through three stages. At the last stage of the collapse induced by  $F_p$ , for high-viscosity ferrofluid, the interfacial tension resulted resistance of breakup was stronger than water. As a result, the breakup takes longer time, and the ferrofluid droplets are larger than in the case of low-viscosity water.



**Fig. 5** a Water and b ferrofluid droplet sequences under various flow rate ratios. c Size of water and ferrofluid droplets as a function of flow rate ratio. The dash lines are given for visual guidance

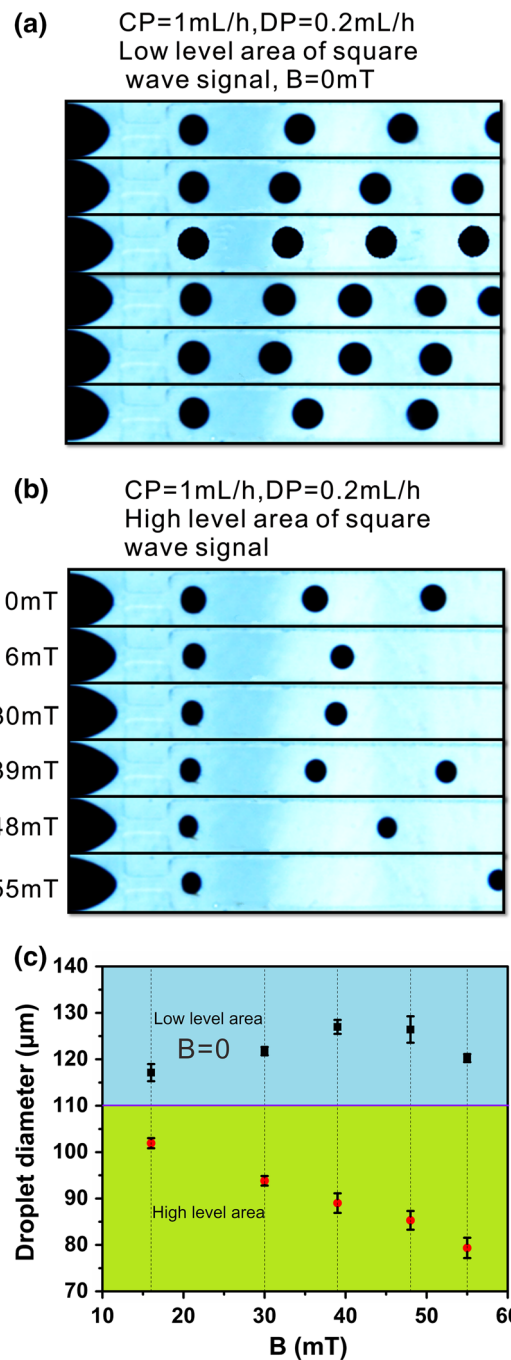
As  $Q_o/Q_i$  goes on increasing (area II, Fig. 5c), the droplet sizes of both water and ferrofluid decrease slowly, which means the larger the flow rate ratio, the smaller the dependence of droplet size on  $Q_o/Q_i$ .



**Fig. 6** Maximum contraction position of ferrofluid tip. **a** Illustrations without magnetic field and **b** with magnetic field. **c** Maximum contraction position as a function of magnetic flux density and comparison with droplet size (*inset 2*) and various forces the ferrofluid tip suffered in the droplet formation progress with magnetic field (*inset 1*)

Higher magnetic flux density leads to a higher-viscosity ferrofluid, and higher viscosity of dispersed phase results in an increase in the droplets size (Nie et al. 2008). In contrast to our results, it was found that magnetism plays another role in the formation of ferrofluid droplet.

In squeezing regime, dispersed phase occupies almost the whole throat and continuous phase flows hardly. Thus, the pressure increases dramatically at the region outside ferrofluid thread. Continuous phase starts to squeeze the dispersed phase and a neck induced. Till the neck collapses, droplet breaks up. Continuous phase flows through the orifice freely. When local field is applied on the upstream, the additional magnetic force  $F_m$  ( $F_m = \mu_0 M \nabla H$ ,  $\mu_0$  is the magnetic permeability of free space,  $M$  is the magnetization, and  $\nabla H$  is the gradient of the external magnetic field strength) (Fig. 6c, inset 1) starts to drag the tip from moving downstream, which leads to a jam at the outlet of the throat. Continuous phase flows through the throat more difficult. Pressure in continuous phase increases faster than the situation without magnetic field. The thinning process of the neck speeds up, which causes the droplet breakup earlier. A relatively smaller droplet is induced. At the moment of droplet breakup, velocity of a new ferrofluid tip and droplet is opposite. A maximum contraction position of ferrofluid



**Fig. 7** Droplet formation under square wave magnetic field. **a** Low-level sequences, **b** corresponding high-level sequences, **c** sizes of ferrofluid droplets as a function of magnetic flux density in the two areas of square wave signal

tip exists before the next droplet starts to form. Figure 6 shows the maximum contraction position of ferrofluid tip under various magnetic flux densities. Distance between the maximum contraction position of ferrofluid tip and the entrance of throat ( $C_{max}$ ) firstly decreases with the increasing in magnetic flux density and then nearly keeps constant,

which is similar to the trend of droplet size (Fig. 6c, inset 2). Shorter distance to the entrance of throat leads less time to form the next droplet. Thus, droplet formation frequency increases, and the size decreases.

Magnetoviscous effect results in an increase in droplet size, and magnetic drag effect performs oppositely. It was found that the average size of the droplets decreased with applied magnetic field, which predicted the magnetic drag played a more important role than the magnetoviscous effect. When  $B$  reached nearly 60 mT, droplets generated fast enough, the size of the droplets became stable due to the couple effect of magnetic drag and surface tension.

### 3.3 Controlling the size of the droplet by using square wave magnetic field

Here, the average size of the droplets can be periodically controlled by using square wave signal (Fig. 7). Figure 7c shows the relationship between the diameter and the applied square wave signal. At the high-level area of the signal, droplet size decreases with the increasing magnetic flux density for the reason that magnetic drag force accelerates the droplet breakup. At the same time, magnetic drag force resists the flow of ferrofluid driven by syringe pumps. Inner pressure of ferrofluid grows. When signal goes to the low level, magnetic drag force is disappeared and the pressure decreases between inside and outside of ferrofluid which promotes the flow. The inner phase flows faster than pump actuating speed; thus, bigger droplets are generated. Increasing magnetic flux density leads to an increase in released pressure and thus leads to an increase in droplets size. To this end, magnetic droplets with different size distribution could be periodically obtained by varying the characteristics of the square wave magnetic field.

## 4 Conclusions

In this work, magnetic field was applied to realize actively controllable generation of ferrofluid droplets in flow-focusing geometry. The average size of the droplets could be simply controlled by varying the intensity of the magnetic field. The breakup dynamics of droplet with magnetic interaction were studied. In comparison with magnetoviscous effect, magnetic drag force played a more important role in the droplet formation process. It was found that maximum contraction distance of the tip was proportional to the droplet size in squeezing regime. Moreover, the square wave magnetic field could be used to periodically generate droplets with different sizes. These results provide new insight into the formation dynamics of ferrofluid droplets under a controlled external force and supply a new way to produce bulk monodisperse droplets with different sizes.

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